## **Polymerisation Reactions**

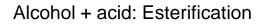
# Distinguishing features of Chain- and Step-Polymerisation mechanisms:

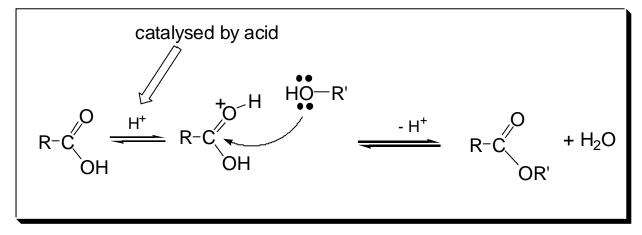
| Chain polymerisations                      | Stepwise polymerisation =              |
|--|--|
| (Vinyl monomers)                           | "polycondensation"                     |
| Reactive chain end adds monomer            | Any two molecular species can react    |
| units one at a time                        |  |
|  |  |
| Monomer concentration decreases            | Monomer disappears early in the        |
| steadily throughout reaction               | reaction:                              |
|  | <u>at DP = 10 less than 1% monomer</u> |
|  | <u>remains</u>                         |
| High-molecular weight polymer is           | Polymer MW rises steadily, rapid       |
| formed at once, MW changes little          | increase only in last stages of        |
| throughout reaction                        | reaction                               |
|  |  |
| Long reaction times increase yields        | Long reaction times essential for high |
| but not molecular weight                   | mol. weight                            |
|  |  |
| Reaction mixture contains only             | At any stage monomer, oligomers,       |
| monomer, high-MW polymer, 10 <sup>-8</sup> | polymers present. All molecular        |
| parts of growing chains                    | species contribute to growth.          |

### **Step Polymerisation Reactions**

<u>Condensation reactions of di-carboxylic acids</u>: most important reaction for the preparation of polymers by stepwise reactions.

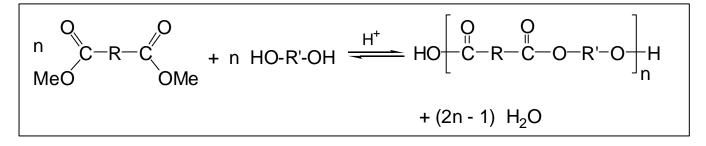
#### Polyesters





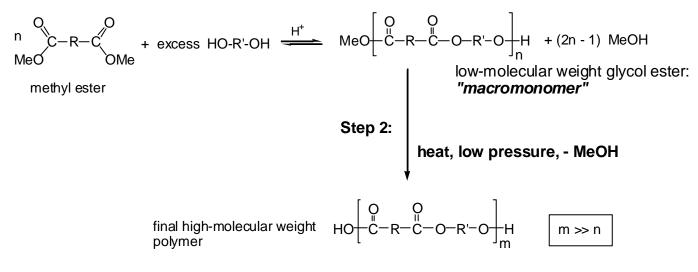
The reaction is an equilibrium. In order to get good yields, the water must be removed.

Using di-basic acids and diols gives polymers:

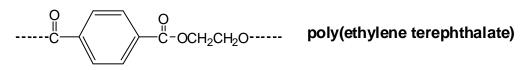


In practice, the equilibrium is not very favourable and water is difficult to remove. Polyesters are therefore made in a two-step process:

#### Step 1:

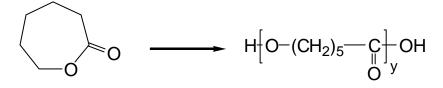


Linear aliphatic polyesters have low melting points and high solubility and are not useful. Stiffer building blocks give high-melting polymers:



for films, plastic drinks bottles, etc.

Homopolymerisation of cyclic esters is also practised:

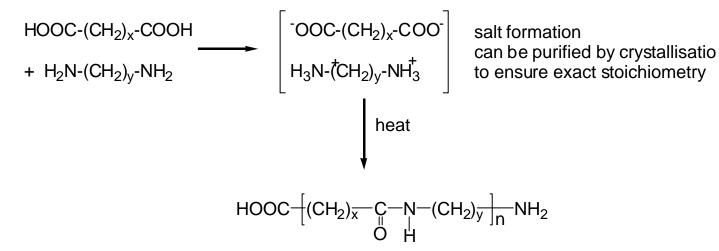


carpolactone

#### **Polyamides**

Homopolymerisation of  $\omega$ -aminoacids:

Condensation of diacids with diamines:

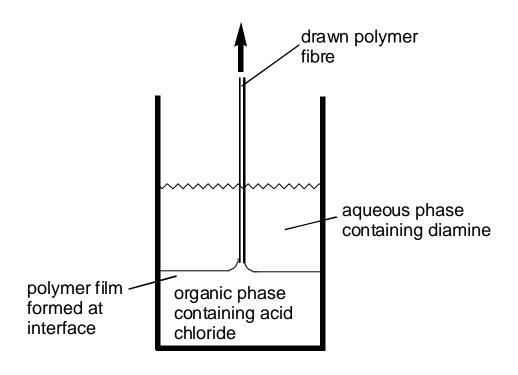


If x = 4 and  $y = 6 \rightarrow Nylon-66$ launched nylon production from 1935 high melting (mp. 265°C), pliable, silk-like fibre

Condensation of acid chlorides with diamines:

 $\begin{array}{cccc} \text{CIOC-}(\text{CH}_2)_{x}\text{-}\text{COCI} & \longrightarrow & \text{HOOC-}\left[(\text{CH}_2)_{\overline{x}}\text{-}\underset{O}{\overset{H}{\overset{H}}}\text{-}_{H}(\text{CH}_2)_{\overline{y}}\right]_{n}\text{NH}_2 \\ & + & \text{H}_2\text{N-}(\text{CH}_2)_{y}\text{-}\text{NH}_2 & + & 2n \text{HCI} \end{array}$ 

Acid chlorides are much more reactive. Polymers can be made at room temperature: Interfacial condensation:



Natural polyamides:

- Polypeptides
- ♦ Wool
- ♦ Silk

#### **Kinetics of Step Reactions**

In a polyester formation, the disappearance of –COOH groups can be described by the equation:

$$\frac{-d [COOH]}{dt} = k [COOH][OH]$$

**Definitions:** 

 $c_0$  = initial concentration of functional groups,

c = concentration at any given time,

p = progress of the reaction, defined as fraction of functional groups that has reacted at time *t*. It follows;

$$c = c_0(1-p)$$

With bifunctional reactants, if  $N_0$  = initial number of functional groups,

N = number of functional groups at time *t*, then the number-average degree of polymerisation  $DP_n$  is given by:

$$DP_n = \frac{N_0}{N} = \frac{c_0}{c} = \frac{1}{1 - p}$$

"Carother's equation"

Since all monomers can grow at the same time, the reaction gives oligomers <u>unless very high conversions</u> are achieved.

| p     | DPn  |
|-------|------|
| 0.90  | 10   |
| 0.95  | 20   |
| 0.99  | 100  |
| 0.999 | 1000 |

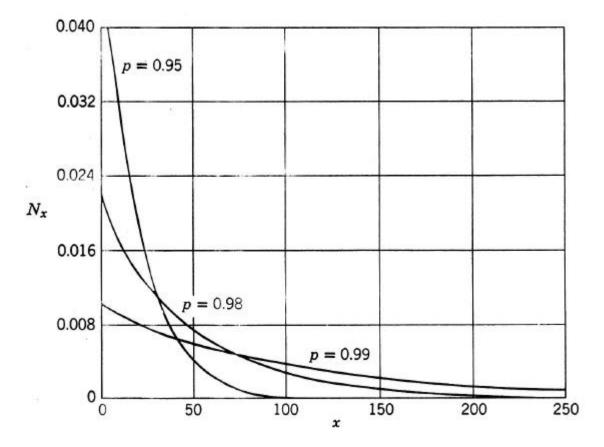
Since [COOH] = [OH], the rate equation becomes:

$$-dc/dt = kc^2$$

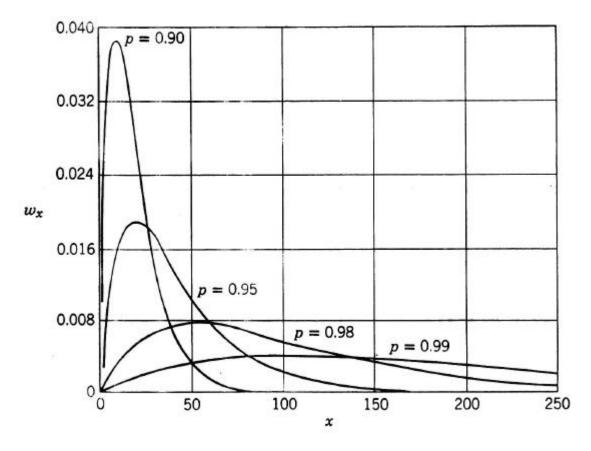
Integration:

$$c_0 kt = \frac{1}{1 - p} + \text{const.}$$
  
 $\Rightarrow DP_n$  increases linearly with reaction time

Mol-fraction distribution of chain molecules in a linear step-reaction polymer for several extents of reaction p:



Weight fraction distribution:

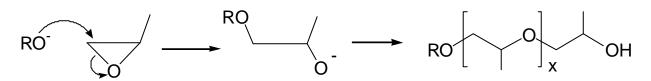


→ In a step-polymerisation, where the polymerisation is an equilibrium reaction, the reaction needs to go to very high convertion (>> 99.9%) to achieve a high molecular weight.

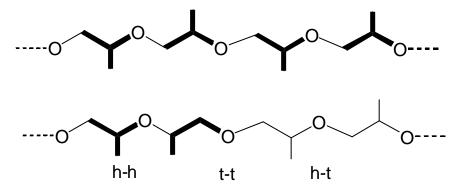
Since step reactions are equilibria, a large polymer chain is subject to attack and "back-biting" → ring formation Needs to be avoided by control of stoichiometry and reaction conditions, e.g. avoid exposure to catalyst once monomers have been consumed.

#### Other step polymerisations:

#### Epoxide polymerisation

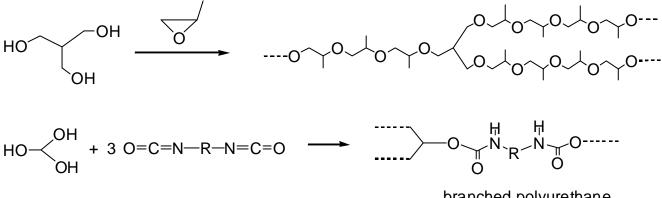


Large scale polymerisation of propylene oxide. **Regioisomers:** 



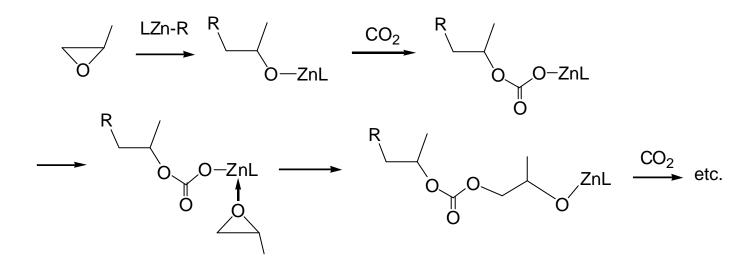
Epoxides are also polymerised cationically and by a coordination mechanism.

With tri-functional alcohols, branched products are produced polyurethane products

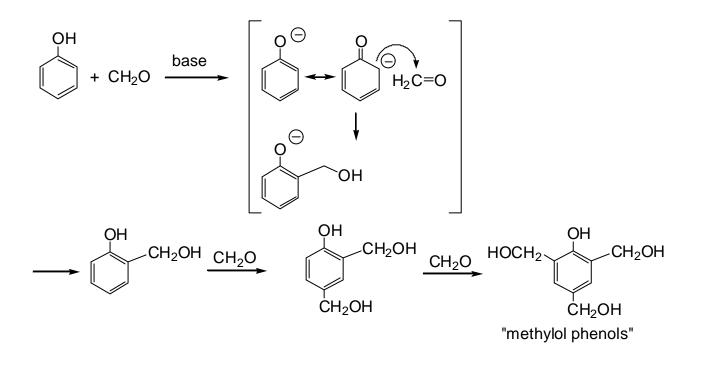


branched polyurethane

#### Epoxide / CO<sub>2</sub> copolymerisation to polycarbonates:



#### Phenol-Formaldehyde Resins:



Further condensation catalysed by acids or bases gives methylene-bridged networks: →thermosets

