# UNIVERSITY COLLEGE LONDON

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University of London

# **EXAMINATION FOR INTERNAL STUDENTS**

For The Following Qualification:-

B.Sc.

**Biochemical Eng E126: Introduction to Bioprocess Design Principles** 

COURSE CODE	: BENGE126
UNIT VALUE	: 0.50
DATE	: 05-MAY-05
TIME	: 14.30
TIME ALLOWED	: 3 Hours

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# **TURN OVER**

## PART A

1.

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The Reynolds number is dimensionless and is used to define the balance between which forces that act during flow of fluid in a pipe? [5]

Define the Reynolds number for pipe flow.

Calculate the flow velocity needed for water being pumped in a circular pipe of 5cm radius to be:

a) Laminar

b) Turbulent

[5]

[5]

What is the MOODY chart? Sketch one and indicate the key axes and regions of interest on it. [10]

## 2.

State the equations and correlations used in order to estimate the pressure drop in a packed bed. Defend the validity of the assumptions on which these equations are based. [10]

In adopting a new chromatographic matrix you record a change in pressure drop. The mean particle size has not changed however. What may be contributing to the change in pressure drop across the column? [5]

Using the equations and correlations you have identified above estimate the size of particle that will result in a pressure drop of 2.5 bar. Do you feel that this is an acceptable set of conditions to operate under?

Flowrate: 150 L/h Column radius: 30 cm Bed height: 15cm

List any assumptions that you make in addition to those covered in the first part of the question. [10]

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A process development team intends to use centrifugation to recover an intracellular protein from yeast homogenate. Some of the background information is given below.

- a) Calculate the mass balance and evaluate the centrifuge performance. [15]
- b) If the yield is lower than 95%, determine the amount of buffer needed to achieve 95% yield using a washing stage. [10]

### **Background** information

3.

Homogenate volume: 1000L Debris concentration: 100g/L Product concentration: 1 g/L Soluble contaminants concentration: 65 g/L Centrifuge carry over: 5% Centrifuge dewatering level: 50% Assume for the purposes of calculation that the density of the cells and the liquor are the same at 1kg/L.

- 4. A membrane system was used to recover an intracellular protein from 1000L of yeast homogenate. Debris concentration is 100g/L. It started with concentration process to 500L in the retentate tank and the yield was 30%. To increase the yield, 1000L of buffer is available for a diafiltration process. Assume for the purposes of calculation that the density of the cells and the liquor are the same at 1kg/L.
- a) Calculate the mass balance of the entire process. [15]
- b) If the target for yield is 90%, how can the process operation be altered to meet the target without using additional buffer? [10]

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Determine whether the following stereoisomers A and B are R or S a) isomers



A newly identified enzyme is able to convert A and its enantiomer A2 into products X and Y. After 50% of a racemic mixture of A and A2 was converted, the product was obtained as 94% X and 6% Y.



b)	Calculate the enantiomeric excess of product X	[2]
c)	Calculate the E-value $(E_R)$ for the reaction.	[4]

You may find the following formula useful in your calculations:

$$E_R = \frac{\ell_n \left[ 1 - c \left( 1 + ee_p \right) \right]}{\ell_n \left[ 1 - c \left( 1 - ee_p \right) \right]}$$

### **CONTINUED**

[4]

c)

d)	Using a graphical method, determine whether this enzyme is suitable to obtain $X$ with an enantiomeric excess of 0.95	[10]
e)	Briefly describe an enzyme engineering strategy to obtain Y with an enantiomeric excess of 0.95.	[5]
6.		
	This question concerns the operation and control of biocatalytic reactors.	
a)	What are the four key parameters to be controlled in an industrial biocatalytic conversion?	[4]
b)	Explain why they need to be controlled.	[7]
c)	What methods are available for the control of these parameters?	[4]
d)	Explain in detail the process development implications of implementing these methods.	[10]

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## **END OF PAPER**

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