

**UNIVERSITY COLLEGE LONDON**

University of London

**EXAMINATION FOR INTERNAL STUDENTS**

For The Following Qualifications:-

*B.Eng.*    *B.Sc.*    *M.Eng.*

**Biochemical Eng E100: Introduction to Biochemical Engineering**

COURSE CODE            :   **BENGE100**

UNIT VALUE             :   **0.50**

DATE                     :   **06-MAY-04**

TIME                     :   **14.30**

TIME ALLOWED         :   **2 Hours**

**Answer THREE QUESTIONS. Only the first three answers given will be marked.**  
**ALL questions carry a total of 25 MARKS each, distributed as shown [ ]**

1. By reference to a specific example outline the main technical and economic issues that must be considered in the creation of a new drug therapy for HIV – AIDS. [25]
  
2.
  - i) Describe the various methods available for sterilisation, their mechanism of cell inactivation and their application in an industrial fermentation facility. [13]
  - ii) Outline the principles of sterile operation and the design features associated with the sterile operation of a fermentation process. [12]
  
3.
  - i) The maximum specific growth rate ( $\mu_{\max}$ ) for a microorganism grown by batch culture in a complex media is  $1.4 \text{ h}^{-1}$ . Calculate the doubling time ( $t_d$ ) for the microorganism under such conditions. Give typical  $t_d$  values for bacteria and mammalian cells in culture. [10]
  - ii) Describe the various different modes of operation of cell culture processes. [7]
  - iii) Describe the various patterns of growth and product formation for cultured microorganisms. Explain why this information is important for process design. [8]

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4.

A bacterium was grown aerobically on glucose as the limiting substrate to produce biomass and a recombinant product. The working volume of the fermenter was 50 litres and the final dry biomass concentration was  $10\text{g l}^{-1}$ . The biomass and product formulas are  $\text{CH}_2\text{O}_{0.5}\text{N}_{0.2}$  and  $\text{CH}_{1.7}\text{O}_{0.3}\text{N}_{0.3}$  respectively. Given that ammonia was used as the nitrogen source and that the synthesis of the recombinant product is growth-associated:

- i) Write down a general stoichiometric equation for biomass and recombinant product synthesis. Clearly state any assumptions made. [10]
- ii) Calculate the stoichiometric coefficients in the equation for biomass, glucose and product given that the cells contain 5% w/w ash. The yields of biomass and of product on glucose are 0.55 and 0.2, respectively. [15]

5.

- i) Outline the cellular requirements for oxygen in an aerobic fermentation process and the stages involved in the transport of oxygen from a gas bubble to the site of utilisation within the cell. [12]
- ii) Calculate the saturation concentration of oxygen,  $C^*$ , in a fermentation broth at the base and the liquid surface of a  $10\text{ m}^3$  fermenter ( $h = 4.85\text{ m}$ ,  $d = 1.62\text{ m}$ ). You may assume that the space utilisation is 80% v/v and that the concentration of oxygen in the outlet gas is 17.5% v/v. The value of Henry's Law coefficient under the conditions of operation is  $27.5\text{ bar m}^3\text{ kg}^{-1}$ . Clearly state any further assumptions made. [13]

**END OF PAPER**