Structure of Matter

Problem Sheet 1 Answers

1. (a)
$$N = \frac{PV}{k_B T} = \frac{0.5 \times 10^3}{1.38 \times 10^{-23} \cdot 300} = 1.22 \times 10^{25}$$

(b) $V = \frac{N_m RT}{P} = \frac{3 \times 8.31 \times 263}{10^2} = 65.6 \text{ m}^3$
(c) $V = \frac{8.31 \times 273}{1.01 \times 10^5} = 0.0224 \text{ m}^3 = 22.4 \text{ litres} = 22,400 \text{ cc}$

- 2. $P = Nk_BT/V = nk_BT$, so $P_e = P_i = 5 \cdot 10^{19} \times 1.38 \cdot 10^{-23} \times 10^8 = 6.9 \cdot 10^4$ Pa
 - $P_{Total} = P_e + P_i = 1.38 \cdot 10^5 \text{ Pa} = 1.37 \text{ atmospheres}$

$$U_i = U_e = \frac{3}{2}Nk_BT = \frac{3}{2}PV = \frac{3}{2} \times 6.9 \cdot 10^4 \times 10^3 = 1.03 \cdot 10^8 \text{ J}$$

$$U_{Total} = U_i + U_e = 2.07 \cdot 10^8 \text{ J}$$

3. (a)



Figure 1: default

(b) Using
$$\frac{P_1V_1}{T_1} = Nk_B = \text{constant}$$
, so
(1) $\frac{1 \cdot 0.5}{300} = \frac{1.5 \cdot 0.5}{T_1} \rightarrow T_1 = 450 \text{ K} \rightarrow \Delta T = 150 \text{ K}$
(2) $\frac{1.5 \cdot 0.5}{450} = \frac{1.5 \cdot 1}{T_2} \rightarrow T_2 = 900 \text{ K} \rightarrow \Delta T = 450 \text{ K}$
(3) $\frac{1.5 \cdot 1}{900} = \frac{1 \cdot 1}{T_3} \rightarrow T_3 = 600 \text{ K} \rightarrow \Delta T = -300 \text{ K}$
(4) $\frac{1 \cdot 1}{300} = \frac{1 \cdot 0.5}{T_4} \rightarrow T_4 = 300 \text{ K} \rightarrow \Delta T = -300 \text{ K}$
(c) $\Delta U = \frac{3}{2}Nk_B(T_1 - T_0) = \frac{3}{2}(P_1V_1 - P_0V_0)$ so,

(1)
$$\Delta U = \frac{3}{2}(1.5 * 1.01 \times 10^5 * 0.5 - 1.0 * 1.01 \times 10^5 * 0.5) = 3.79 \times 10^4 \text{ J}$$

- (2) $\Delta U = \frac{3}{2}(1.5 * 1.01 \times 10^{5} * 1.0 1.5 * 1.01 \times 10^{5} * 0.5) = 11.36 \times 10^{4} \text{ J}$ (3) $\Delta U = \frac{3}{2}(1.0 * 1.01 \times 10^{5} * 1.0 - 1.5 * 1.01 \times 10^{5} * 1.0) = -7.64 \times 10^{4} \text{ J}$ (4) $\Delta U = \frac{3}{2}(1.0 * 1.01 \times 10^{5} * 0.5 - 1.0 * 1.01 \times 10^{5} * 1.0) = -7.64 \times 10^{4} \text{ J}$ (d) $\Delta U_{total} = 0$ (take care of rounding errors!) (e) $\Delta W = -\int P dV$ (1) $dV = 0 \rightarrow \Delta W = 0$ (2) P = cont, so $\Delta W = -P \Delta V = -1.5 * 1.01 \times 10^{5} * (1.0 - 0.5) = -7.57 \cdot 10^{4} \text{ J}$ (3) $dV = 0 \rightarrow \Delta W = 0$ (4) $\Delta W = -P \Delta V = -1.0 * 1.01 \times 10^{5} * (0.5 - 1.0) = 5.05 \cdot 10^{4} \text{ J}$ (f) So ΔW by gas $= -7.57 \cdot 10^{4} + 5.05 \cdot 10^{4} = 2.52 \cdot 10^{4} \text{ J}$
- (g) In each stage heat enters or leaves the system (as well as the work done). During part (1) and (2) heat must have been put into the system.

(h) The work done is the area bounded by the path in the PV diagram.



- 5. (a) Blocks end up at same temp T and have same change in heat, so $C(T-323)*5+C(T-273)*10=0 \quad \to \quad 15T=(273*10)+(323*5)$
 - $\rightarrow T = 289.7 \text{K} = 16.7^{\circ} \text{C}$ (b) Mass exhaled each breath = $0.5 * 1.3 \times 10^{-3} = 6.5 \times 10^{-4} \text{ kg}$
 - Energy lost per breath = $1020 * 6.5 \times 10^{-4} * (37 20) = 11.3 \text{ J}$ Total per hour = 11.3 * 20 * 60 = 13.6 kJ (equivalent to 3.8 W)
 - (c) Heat flow due to radiation = $\sigma(T_1^4 T_2^4) * A = 5.67 \times 10^{-8} (308^4 293^4) * 5 \times 10^{-2} = 4.6$ W So heat loss in one hour = 4.6 * 3600 = 16.6 kJ

(d) Total energy change = 50 * 100 * 360 =
$$1.8 \times 10^7$$
 J
So $\Delta T = \Delta Q/C = \frac{1.8 \times 10^7}{1020 * 1.3 \times 10^{-3} * 4 \times 10^6} = 3.4^{\circ}C$

6. (a)
$$dQ = 0$$
 so first law becomes $dU = -PdV = -\frac{Nk_BT}{V}dV$ (using ideal gas EOS)
also $U = \frac{n_d}{2}Nk_BT \rightarrow dU = \frac{n_d}{2}Nk_BdT$
equate the above for $dU \rightarrow -\frac{Nk_BT}{V}dV = \frac{n_d}{2}Nk_BdT$
divide through to get: $\frac{dT}{T} = -\frac{2}{n_d}\frac{dV}{V}$.
(b) $\ln T = -\frac{2}{n_d}\ln V + c_1 = \ln V^{-2/n_d} + \ln c_2 (c_1 \text{ and } c_2 \text{ are constants})$
 $\rightarrow TV^{2/n_d} = c_2$.
(c) Using $c_3 * T = PV \rightarrow P * V * V^{2/n_d} = c_2/c_3 = c_4 (c_3 \text{ and } c_4 \text{ are constants})$
 $\rightarrow PV^{(2+n_d)/n_d} = c_4$
but $\gamma = \frac{C_P}{C_V} = \frac{(\frac{n_d}{2}Nk_B + Nk_B)}{\frac{n_d}{2}} = \frac{n_d + 2}{n_d}$
So $PV^{\gamma} = c_4$ For ideal gas $n_d = 3$, so $\gamma = 5/3$
(d) $P_1V_1^{\gamma} = P_0V_0^{\gamma} \rightarrow P_1 = P_0(V_0/2V_0)^{\gamma} = P_0(1/2)^{5/3} \approx 0.315P_0$
For isotherm, $P_1V_1 = P_0V_0 \rightarrow P_1 = P_0(V_0/2V_0) = 0.5P_0$
So adiabat is steeper than the isotherm.



Figure 5: Isotherm and adiabat

7. (a)
$$dQ = 0 \to dW = dU = C_V dT$$

 $\to \Delta W = \int W = \int U = C_V (T_1 - T_0)$
(b) $\Delta W = -\int P dV = -\int AV^{-\gamma} dV = -\frac{A}{1-\gamma} \left[V^{1-\gamma}\right]_{V_0}^{V_1}$
where A is a constant, but $AV^{-\gamma} = P$, so
 $\Delta W = \frac{1}{(\gamma - 1)} \left[P_i V_i\right]_0^1 = \frac{1}{(\gamma - 1)} (P_1 V_1 - P_0 V_0)$
(c) $\gamma - 1 = (n_d + 2)/n_d - 1 = 2/n_d$, so
 $\Delta W = \frac{1}{(\gamma - 1)} (P_1 V_1 - P_0 V_0) = \frac{Nk_B}{2/n_d} (T_1 - T_0) = (n_d N k_B/2) (T_1 - T_0)$
 $\to \Delta W = C_V (T_1 - T_0)$ as before

8. (a)
$$v_s = \sqrt{\frac{\gamma P}{\rho}} \rightarrow \gamma = \frac{n_d + 2}{n_d} = \frac{\rho v_s^2}{P} = \frac{nmv_s^2}{nk_BT}$$

 $n_d + 2 = n_d \frac{mv_s^2}{k_BT} \rightarrow n_d \left(\frac{mv_s^2}{k_BT} - 1\right) = 2$
 $\rightarrow n_d = 2 \left(\frac{mv_s^2}{k_BT} - 1\right)^{-1}$
(b) $n_d = 2 \left(\frac{4.82 \times 10^{-26} \cdot 344^2}{1.38 \cdot 10^{-23}293} - 1\right)^{-1} \approx 5$

(c) air is mostly diatomic, so might expect $n_d = 7$, but reason is explained in lec. 7